From: Stuble, Bil

To: Vandendoren, Alain; Brichacek, Todd; Potter, Dolly; Morris, Cliff; Branson, Eric; Slaybaugh, Kip; Hodgson, Rich

Subject: SNCR Report / NOxOUT A Consumption AUGUST Date: Tuesday, September 26, 2006 3:53:48 PM

Attachments: SNCR monthly report.xls

The SNCR system ran 722 hours in August and consumed 29,068 lbs urea solution. There were no deliveries in August. Costs details are reported as attached and compared to June and July.

In August, using the latest ammonia slip measurement from the stack test on August 8 (11 ppm dry basis, 14.7 ppm wet), there was good balance between NH3 in and NH3 out plus NH3 reacted with NOX.

The process shall be tuned up -- the best opportunity is in improving the furnace and calciner temperature control. Fuel Tech instrumentation shows the urea consumption spiking at high furnace temperatures.

Note the percentage NOx reduction achieved by SNCR in August -- again did not meet quite design. It was 34% versus 35% design.

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UREA NOXout A Monthly Report

Coal Stoker Furnace SNCR Process Name: NOxOUT A

for Calciners CA-1 and CA-2 Reagent: Urea

Note: Monthly and annual numbers assume 85% onstream

8/7/2006

SNCR startup date CA-2: 6/13/06

	Actual	Actual	Actual	vs Design
All numbers "per furnace" basis.	June, 2006	July, 2006	August, 2006	Fuel Tech Proposal
All humbers per jurnace busis.	<u>CA-2</u>	CA-2	<u>CA-2</u>	& Calcinator 080105
	Typical or Est Measured	Typical or Est Measured	Typical or Est Measured	<u>Design</u>
days	30	31	31	<u> </u>
PROCESS Calciner Ore Feed Rate, tORE/h	115	99	114	140
Furnace Heat Load MM Btu/Hr	133	128	141	155
Furnace Outlet Temp deg F	1680	1680	1690	1718
non-SNCR controlled NOX, lb/MM Btu	0.39	0.41	0.41	0.45
non-SNCR controlled NOX, lb/hr non-SNCR controlled ppm NOX	51.9	52.6	57.8	69.8 231
non-SNCR controlled NOx, tNOX/y	193	196	215	260
SNCR controlled NOX, lb/MM Btu	0.250	0.270	0.270	0.293
SNCR controlled NOX, lb/hr	33.3	34.6	38.0	45.3
SNCR controlled NOx, tNOX/y	124	129	142	169
SNCR NOX reduction, %	35.9	34.1	34.1	35.0
NOX reduction tNOX/y	69	67	73	91
Nox - Urea - NH3 Balance Check				
Ammonia slip, ppm, furnace outlet	2.5	2.5	147	15.0
Ammonia slip, ppm, stack outlet Ammonia Slip, % of urea consumption	2.5 3.1	2.5 2.5	14.7 19.9	14.9 6.9
<u>In</u> Urea feed, pure urea, lb/hr	20.8	24.4	20.1	65.6
Converted to NH3, lb/hr	11.8	13.8	11.4	37.2
Total NH3 in, lb/hr	11.8	13.8	11.4	37.2
<u>Out</u>				
Ammonia Slip, lb/hr Ammonia reacted w / NO, lb/hr	0.6 7.0	0.6 6.8	4.0 7.5	4.5 9.2
Total NH3 out, lb/hr	7.7	7.4	11.5	13.8
Nox - Urea Balance Check Forget ab	oout Slin			
Torget at	<u> </u>			
<u>In</u> Urea feed, pure urea, lb/hr	20.8	24.4	20.1	65.6
Total Urea in, lb/hr	20.8 20.8	24.4	20.1 20.1	65.6
Out				
Urea reacted w / NO, lb/hr	18.6	18.0	19.7	24.4
Total Urea out, lb/hr	18.6	18.0	19.7	24.4
UREA USAGE				
Urea sol'n consumption, lbUREA/month	11,622	32,897	29,068	81,413
SNCR hours of operation / month Urea consumption, lb/h	280 42	674 49	722 40	621 131
Urea consumption, gal/h	4.4	5.1	4.2	13.8
Urea consumption, gal/y, annualized	32,499	38,215	31,522	102,755
Urea cost, \$/gal delivered	1.52	1.52	1.52	1.49
COSTS Urea cost, \$/lb solution delivered	0.16	0.16	0.16	0.157
Urea cost, \$/ton solution delivered	319.74	319.74	319.74	313.43
Urea cost, \$/month Urea cost, \$/tORE	1,858 0.06	5,259 0.08	4,647 0.06	12,759 0.15
Urea cost, \$/ton Nox removed	713	869	652	1,685
Furnace CO limit, ppm	na	na	na	500
Furnace Exhaust, lb/hr	258,913	249,724	274,300	301,741
Furnace Exhaust, ACFM Stack Exhaust, lb/hr	309,832 257,517	298,835 248,377	328,244 272,821	361,082 300,114
Pure urea consumption, lb/hr	20.75	24.40	20.13	65.60
lb NH3 required / lb NO				
lb/hr NH3 required in "complete" reaction NOX reduction lb/hr	18.6	18.0	19.7	24.4
				•

Urea cost, \$/year per calciner	49,398	58,087	47,914	153,105	l
Urea composition %	50.0	50.0	50.0	50.0	
-	1.14	1.14	1.14	1.14	
Urea spec gravity	9.51			9.51	
Urea lb/gal	9.51	9.51	9.51	9.51	
Fuel Teel Centerts					
Fuel Tech Contacts	Michael Dispett	1	h	-1	
	Michael Bisnett mi 805-983-2655	<u>bisnett@fuelte</u> m	<u>bisnett@fuelte</u>	Cn.com	
	Penelope Stamatakis 630-845-4462				
	030-843-4402				
CDI Contacts	Luis D. Cervantes, Jr. 1	da@aammantaa dl	da@aamrantaa d	olgodo gom	
<u>CDI Contacts</u>	Cervantes~Delgado Inc		deweervantes-d	elgado.com	
	Ph: (714) 990-3940	•			
	Fax: (714) 990-4073				
Stoichiometry					
Stolemonicaly					
MOLECULAR WEIGHTS					
Na2CO3-NaHCO3-2H2O	226.03	226.03	226.03	226.03	
Na2CO3	105.99	105.99	105.99	105.99	
H2O	18.02	18.02	18.02	18.02	
CO2	44.01	44.01	44.01	44.01	
C	12.01	12.01	12.01	12.01	
Air	28.85	28.85	28.85	28.85	
N2	28.01	28.01	28.01	28.01	
O2	32.00	32.00	32.00	32.00	
H2	2.02	2.02	2.02	2.02	
Na	22.99	22.99	22.99	22.99	
S	32.64	32.64	32.64	32.64	
SO2	64.64	64.64	64.64	64.64	
NH3	17.035	17.035	17.035	17.035	
NO	30.01	30.01	30.01	30.01	
CO(NH2)2	60.06	60.06	60.06	60.06	
CO(NH2)2 + H2O	78.08	78.08	78.08	78.08	
2NH3 + CO2 ◀	78.08	78.08	78.08	78.08	
COAHIO HARE				-0.0-	
soCO(NH2)2 lbUREA	60.06	60.06	60.06		lbs urea will produce
makes this many lbAMMONIA (2NH3)	34.07	34.07	34.07	34.07	lbs ammonia
4NH3 + 6NO ———	248.17	248.17	248.17	248.17	
5N2 + 6H2O ◆	248.17 248.17	248.17 248.17	248.17 248.17	248.17	
3N2 + 0H2O	240.17	240.17	240.17	240.17	
and this many lbsAMMONIA (4NH3)	68.14	68.14	68.14	68 11	lbs NH3 will consume
will consume this many lbsNOX (6NO)	180.03	180.03	180.03		lbs NO
win consume and many losivon (01vo)	100.03	100.03	100.03	100.03	TDS INO
Alternate (John Boyle, Fuel Tech)					
NH2-CO-NH2 (Urea) + 2 NO + ½ O2	136.07	136.07	136.07	136.07	
2 N2 + 2 H2O + CO2	136.07	136.07	136.07	136.07	
soCO(NH2)2 lbUREA	60.06	60.06	60.06		lbs urea will consume
will consume this many lbsNOX (2NO)	60.01	60.01	60.01	60.01	lbs NO